Table 6. Kinetic data previously published for growth with and transport of glucose, galactose, maltose, and ribose.

Substrate	Strain	$Ty^a$	$K_x^b \text{ (mg} \cdot L^{-1})$	$\mu_{\text{max}}$ (h <sup>-1</sup> )	$T^c$ (°C)	Reference
Glucose	Н	(1) <sub>S</sub>	4.0	0.94	37	(Monod 1942)
		(2) <sub>S</sub>	8.0	0.65	20	(Jannasch 1968)
	ML30	(3)	0.068 (HA)	0.78	30	(Shehata and Marr 1971)
		(3)	12.6 (LA)	0.03	30	(Shehata and Marr 1971)
	ML308	(4) <sub>S</sub>	2.3	1.23	37	(Koch and Wang 1982)
		(4) <sub>S</sub>	0.10	0.54	37	(Koch and Wang 1982)
	ML30	(5) <sub>S</sub>	0.058	0.82	37	(Senn et al. 1994)
	AB257 (met-)	(6)m	1.8		30	(Villarejo et al. 1978)
	AB257 (met)	(6)m	5.4		30	(Villarejo et al. 1978)
	K12 (BW2901)	$^{(7)}m$	1.1		25	(Death et al. 1993)
Galactose	K12 (KL16)	(8) <sub>S</sub>	108	0.65	37	(Kornberg and Riordan 1976)
	ML32400	$^{(9)}m$	0.72 (LA)		25	(Rotman and Radojkovic 1964)
	ML32400	$^{(9)}m$	0.088 (HA)		25	(Rotman and Radojkovic 1964)
	K12 (D115)	$^{(10)}m$	16 (LA)		21	(Wilson 1974)
	K12 (D115)	$^{(10)}m$	0.09 (HA)		21	(Wilson 1974)
	K12 (W3092)	$^{(11)}d$	0.086		4	(Zukin et al. 1977)
	B/r	$^{(12)}d$	0.063		?	(Quiocho et al. 1979)
Maltose	RV	$(13)_{S}$	8.64	0.76	27	(Dykhuizen and Davies 1980)
	K12 (HfrG6)	$^{(14)}m$	0.32		21	(Szmelcman et al. 1976)
	K12 (HfrG6)	$^{(14)}d$	0.36		21	(Szmelcman et al. 1976)
	K12 (HfrG6)	$^{(15)}d$	0.79		21	(Schwartz et al. 1976)
Ribose	W289	$^{(16)}m$	0.065		37	(David and Wiesmeyer 1970)
	W3092	$^{(17)}m$	0.045		23	(Willis and Furlong 1974)
	W3092	$^{(17)}d$	0.02		?	(Willis and Furlong 1974)

Notes: Explanations to individual reports. (1) Determined by measuring the growth rate in small intervals during retardation phase in batch culture Actual substrate concentrations  $(s_t)$  were calculated with the equation  $s_t = S_0 - S_0(x_t - x_0)/M$ .  $S_0$ , initial substrate concentration;  $x_0$ , initial biomass concentration; x<sub>t</sub>, biomass concentration at time t; M, biomass concentration reached in stationary phase. (2) Determined during chemostat growth at various dilution rates. Glucose concentrations were calculated from biomass concentration and yield data. (3) Determined by measuring growth rates at various initial glucose concentrations in batch culture. The high affinity (HA) K, (68 µg·L<sup>-1</sup>) and µ<sub>max</sub> (0.775·h<sup>-1</sup>) were obtained by Lineweaver–Burk linearization. The low affinity (LA)  $\mu_{max}$  (0.031 h<sup>-1</sup>) was obtained by subtracting the high affinity  $\mu_{max}$  from the maximum specific growth rate observed in batch culture (0.806 h<sup>-1</sup>). Subsequently, the low affinity  $K_s$  was obtained by data fitting using above parameters and a growth model comprising the sum of two Monod terms (Shehata and Marr 1971) (see eq. 7). (4) Determined by measuring growth continuously in a 10-cm flow-through cuvette. The first experiment was carried out with batch- and the second with chemostat-grown cells. (5) Determined according to the same method as presented above for galactose. (6) Determined by measuring of initial uptake rates of [ $^{14}$ C]glucose. Both batch and chemostat grown ( $D = 0.17 \cdot h^{-1}$ ) bacteria were used.  $K_m$  of chemostat-grown cells was approximately three times lower. (7) Determined by measuring initial uptake rates of [ $^{14}$ C]glucose of cells harvested from continuous culture (D = 0.3 h<sup>-1</sup>). (8) Derived from growth rate measurements at various initial galactose concentrations in batch culture. (9) Derived from <sup>14</sup>C]galactose accumulation after incubation of cells for 15 min at various external concentrations. The presence of a low affinity (LA) and high affinity (HA) uptake system was proposed on the basis of a biphasic accumulation pattern. (10) Measured as function of cellular accumulation of [14C]galactose To measure activity of GalP (low affinity proton symport transport system) Mgl (high affinity binding-protein system) was inhibited competitively with β-glycerol-galactoside. (11) Determined by equilibrium dialysis with purified binding protein. (12) Determined by equilibrium dialysis at unknown temperature. (13) Determined in chemostat culture. Steady-state substrate concentrations (s) were estimated from yield data of two identical chemostat runs with different maltose feed concentrations. (14)  $K_{\rm m}$  determined by measuring initial uptake rates (40 s) of [ $^{1}$ H]maltose.  $K_{\rm d}$  was determined by fluorescence titration. (15) Determined by equilibrium dialysis with osmotic shock released binding protein. (16)  $K_{\rm m}$  determined by initial uptake rates (2 min) of [ $^{14}$ C]ribose. (17)  $K_{\rm m}$  determined by measuring initial uptake rates (30 s) of different concentrations of [ $^{14}$ C]ribose.  $K_{\rm d}$  determined by equilibrium dialysis. Type of saturation constant: s,  $K_s$  for growth; m,  $K_m$  for substrate uptake; d,  $K_d$  affinity constants of binding proteins.

Value of saturation constant.

Growth or assay temperature. A comprehensive list of previously published kinetic constants is given in (Lendenmann 1994).

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